

T_1 = Temp of hot reservoir [source]

T_2 = Temp of cold " " [sink]

Q_1 = Heat Supplied to engine

Q_2 = Heat rejected to engine

W = Work done by the heat engine
[$Q_1 - Q_2$]

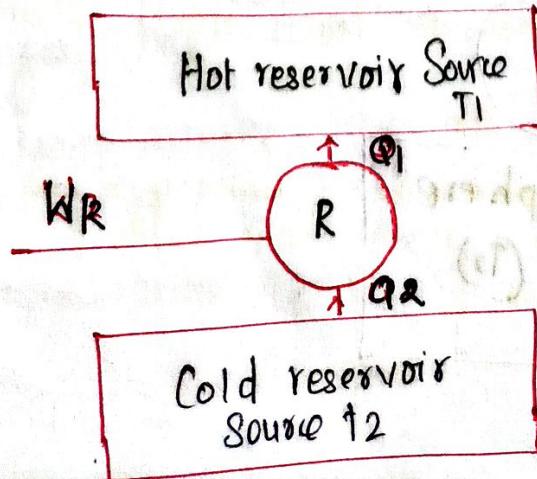
$$\eta_{\text{heat engine}} = \frac{\text{Work done}}{\text{Heat Supplied}}$$

$$= \frac{Q_1 - Q_2}{Q_1} = 1 - \frac{Q_2}{Q_1}$$

$$\frac{T_1 - T_2}{T_1} = 1 - \frac{T_2}{T_1}$$

Refrigerator and heat Pump:

Refrigerator is a device which operates in a cycle maintaining the temp lower than of its Surrounding



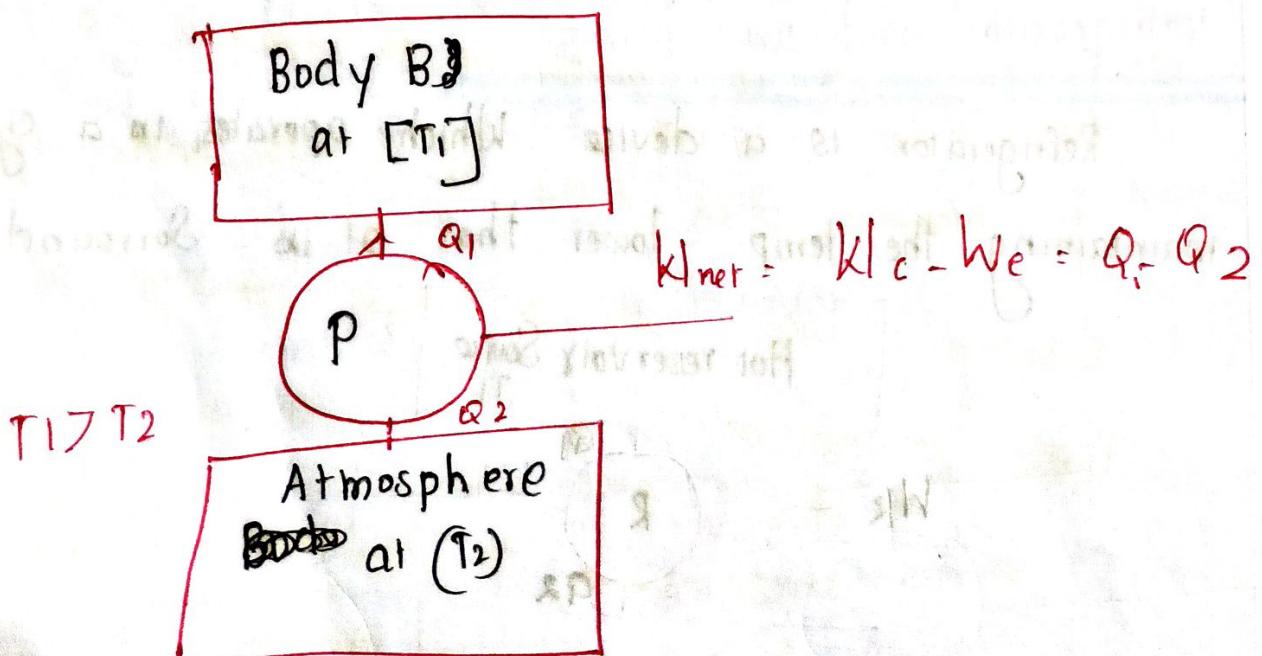
$$C.O.P = \frac{\text{Net Refrigeration effect}}{\text{Work Input}}$$

$$[COP]_{\text{refr}} = \frac{Q_2}{W} = \frac{Q_2}{Q_1 - Q_2}$$

The cold reservoir is refrigerated space and the hot reservoir is atmosphere. The performance parameter is measured by Coefficient of Performance [C.O.P]

$$\text{F.O.P of refrigeration} = \frac{\text{Net refrigeration effect}}{\text{Work Input}}$$

Heat Pump is a device which operating in a cycle maintains a body at a temperature higher than that of its surrounding



The net work is difference b/w

(2-3)

Compressor work and expansion device work

$$\text{C.O.P of heat pump} = \frac{\text{Heat supplied}}{\text{Net work}}$$

$$\text{C.O.P}_{\text{HP}} = \frac{Q_1}{W_1} = \frac{Q_1}{Q_1 - Q_2}$$

$$[\text{COP}]_{\text{HP}} = \frac{Q_1 - Q_2 + Q_2}{Q_1 - Q_2}$$

$$= \frac{Q_1 - Q_2}{Q_1 - Q_2} + \frac{Q_2}{Q_1 - Q_2} = 1 + \frac{Q_2}{Q_1 - Q_2}$$

$$[\text{COP}]_{\text{HP}} = 1 + [\text{COP}]_{\text{ref}}$$

Second law of Thermodynamics

(i) Kelvin - plank Statement

It is impossible to construct a heat engine

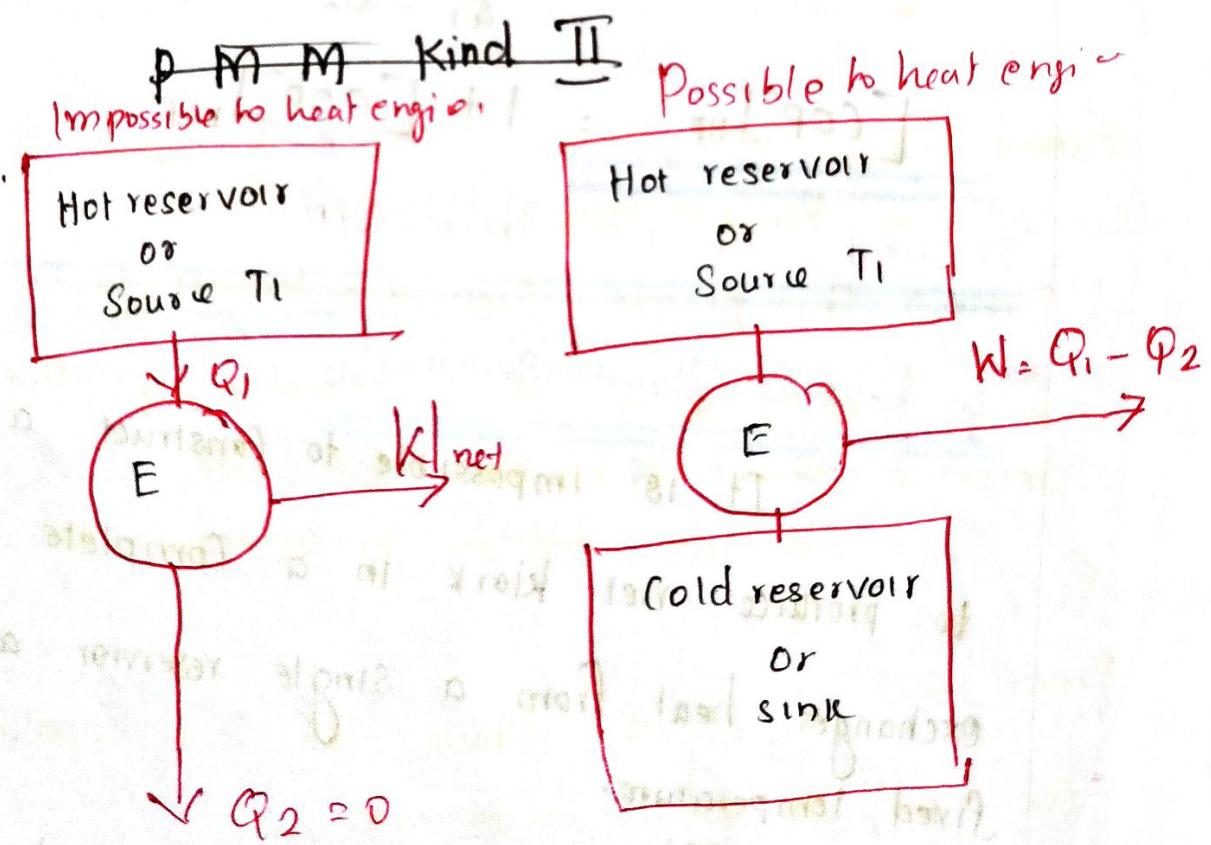
to produce net work in a complete cycle if it exchanges heat from a single reservoir at single fixed temperature.

(ii)

It is impossible to construct a heat engine which will convert all heat energy into equal amount of work in a cyclic process.

- All heat cannot be converted into work.
- Some heat will be rejected to the surroundings

The heat engine must exchange heat with
low temp sink as well as high temp source to keep
operating. The Kelvin-Planck statement can also
be expressed as no heat engine can have thermal
efficiency of 100, or as for a power plant to
operate the working fluid must exchange
heat with the environment as well as the
furnace.



Carnot Cycle and its Performance :

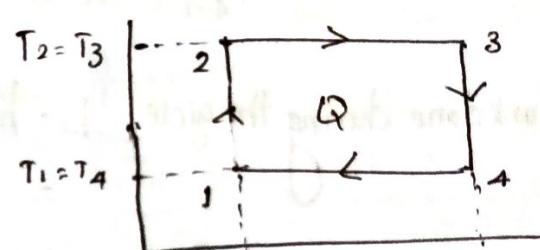
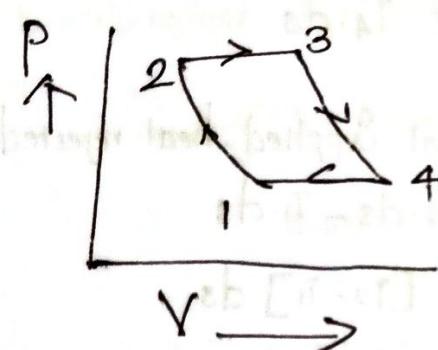
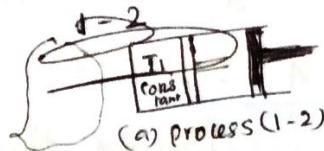
• It is also called as Constant temperature cycle.

• It is introduced by Sadi Carnot

• It consists of 4 Process

(1) Two Isentropic or reversible adiabatic

(2) Two Isothermal Process.



Process 1-2 :

Air Compressed Isentropically from state (1) to (2)

- During this process Pressure & temperature increase from P_1 to P_2 and T_1 to T_2 respectively. But Volume decrease from V_1 to V_2 .
- No heat addition or rejection during this process.

Process 2-3 :

During this Process, the heat Supplied to the fluid at Constant temperature.

- There is no change in temperature $T_3 = T_2$
- Both Volume and entropy increase from V_2 to V_3 and $S_2 \rightarrow S_3$ respectively,

$$\text{Heat Supplied } Q_{S_{2-3}} = T_2 \cdot ds = T_3 \cdot ds$$

$$ds = \frac{dq}{Td} \text{ and } T_2 = T_3$$

Process 3-4:

Air is Isentropically Expanded from State 3 to 4
 Both Pressure and temperature decrease from P_3 to P_4 and
 T_3 to T_4 . But entropy remain constant [$s_3 = s_4$]

Process 4-1:

During this Process, the heat is Isothermally rejected from the fluid and it attain its initial Position.

$$\text{Heat rejected } Q_{4-1} = T_1 \cdot ds = T_4 \cdot ds$$

Workdone during the cycle W_L : heat Supplied - heat rejected
 $= T_2 \cdot ds - T_1 \cdot ds$
 $W_L = [T_2 - T_1] ds$

$$\text{Efficiency of Carnot engine } \eta = \frac{W}{Q_s} = \frac{[T_2 - T_1] ds}{T_2 \cdot ds}$$

$$\eta_{\text{Carnot}} = \frac{T_2 - T_1}{T_2} = \frac{T_H - T_L}{T_H}$$

T_1 and T_2 are minimum and maximum temperature

T_L and T_H are Lower and Higher temp

Heat reservoir:

- Ideal body having large thermal capacity, which either continuously supplies or absorbs the infinite amount of heat without changing its temperature is called thermal energy reservoir.

- If the reservoir continuously supplies heat energy to system,

It is called source.

- If reservoir continuously absorbs heat energy from the system

It is called sink

2.10 An Inventor claim to have developed an efficient heat engine which would have a heat source at 100°C and reject heat to sink at 50°C and give an efficiency 90%. Justify whether his claim is possible or not

Given :

$$T_H = 100^{\circ}\text{C} = 1273\text{ K}$$

$$T_L = 50^{\circ}\text{C} = 323\text{ K}$$

$$\eta = 90\%$$

To find :

whether Inventor's claim is correct or not

Sol :

According to Carnot theorem,

$$\underline{\text{max}} \eta = \frac{T_H - T_L}{T_H} = \frac{1273 - 323}{1273} = 0.76 \\ = 74.6\%$$

max $\eta [74.6\%]$ is less than Proposed Proposed engine

A Carnot engine working b/w 400°C and 40°C

Produce 130 kJ of work Calculate (i) Cycle efficiency
(ii) heat added (iii) entropy changes during heat rejection process

Source Temp = $T_1 = 400 + 273 = 673\text{K} = T_2$
 $(T_1 = T_3)$

Sink Temperature = $T_3 = T_4 = 40 + 273 = 313\text{K}$

Work produced $W_{net} = 130\text{ kJ}$

$$\eta_{Carnot} = \frac{T_1 - T_2}{T_2}$$
$$= \frac{673 - 313}{313} = 53.5\%$$

To find heat added:-

$$\eta_{Carnot} = \frac{k_{net}}{Q_1} = \frac{130}{Q_1}$$

$$Q_1 = \frac{W_{net}}{\eta_{Carnot}} = \frac{130}{0.535}$$

$$Q_1 = 243\text{ kJ}$$

Entropy Change during Heat Rejection Process

$$Q = T_3$$

$$Q_2 = T_3 [S_3 - S_4]$$

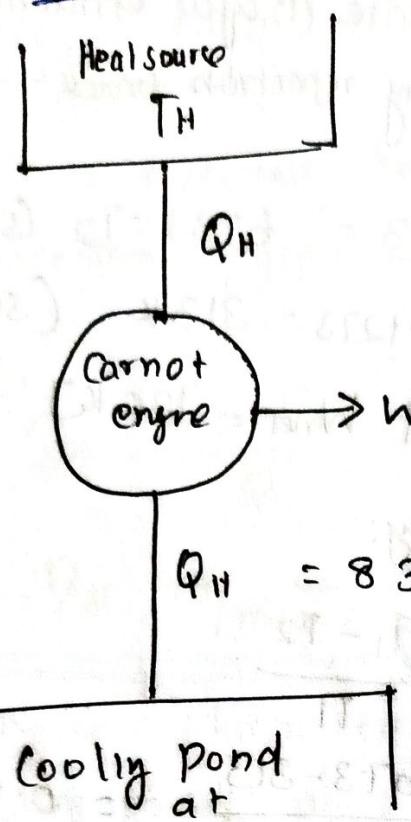
$$S_3 - S_4 = \frac{Q_2}{T_3}$$

$$k_{net} = Q_1 - Q_2$$

$$Q_2 = Q_1 - W_{net} = 243 - 130 = 113\text{ kJ}$$

$$\text{Now } (S_3 - S_4) = \frac{Q_2}{T_3} = \frac{113}{313} = \underline{\underline{0.361\text{ kJ/K}}}$$

$$T_H = \underline{428.5} \text{ K}$$



$$Q_H = 837.2$$

Cooling pond
at

300 K

$$\frac{Q_L}{Q_H} = \frac{T_L}{T_H}$$

$$Q_H = \frac{Q_L}{T_L} \cdot T_H$$

$$= \frac{837.2 \times 428.5}{300} = 1196 \text{ kJ/min}$$

Power developed

$$W = Q_H - Q_L$$

$$= 1196 - 837.2$$

$$= 358.6 \text{ kJ/min}$$

5

(b)

2.21
sem1~~Microcontroller~~

A Carnot engine working b/w 400°C and 40°C produce 130 kJ of work. Calculate (i) cycle efficiency (ii) heat added (iii) entropy changes during rejection process

Spindle

$$\text{Q1} \cdot \text{D} = T_1 = 400 + 273 = 673 \text{ K} = T_2 \text{ (source)}$$

$$T_3 = T_4 = 40 + 273 = 313 \text{ K} \text{ (sink)}$$

$$\text{Work produced } W_{\text{net}} = 130 \text{ kJ}$$

To find Carnot efficiency:-

$$\eta_{\text{Carnot}} = \frac{T_1 - T_2}{T_1}$$

$$= \frac{673 - 313}{673} = 0.585 = 58.5\%$$

To find heat added :-

$$\eta_{\text{Carnot}} = \frac{W_{\text{net}}}{Q_1} = \frac{130}{Q_1} = 0.585$$

$$Q_1 = \frac{130}{0.585} = 222 \text{ kJ}$$

$$Q_1 = 243 \text{ kJ}$$

To find entropy change during heat rejection process

$$Q = Tds$$

$$\text{Heat rejected } Q_2 = T_3 [s_3 - s_4]$$

~~$$W_{\text{net}} = Q_1 - Q_2$$~~

$$S_3 - S_4 = \frac{Q_2}{T_3}$$

$$W = Q_1 - Q_2$$

$$Q_2 = Q_1 - W$$

$$= 243 - 130$$

$$= 113 \text{ kJ}$$

$$\text{Now } (s_3 - s_4) = \frac{Q_2}{T_3} = \frac{113}{313} = 0.357 \text{ J/K}$$

2.7

Case (ii)

$$\eta_{(ii)} = \frac{Q_s - Q_R}{Q_s} = \frac{1120 - 560}{1120} = \frac{0.50}{0.496} = 1.96 \text{ or } 196\%$$

50%.

$(h_{II} = \eta_{max})$ equal so reversible

Therefore, It is reversible heat engine because by II law all the reversible engines have same efficiency

Case (ii) :

$$\eta_{(III)} = \frac{Q_s - Q_R}{Q_s} = \frac{1120 - 108}{1120} = 0.90 = 90\%$$

$\eta_{III} > \eta_{max}$ \therefore It is impossible

- A Carnot engine which rejects heat to a cooling pond at $27^\circ C$ has an efficiency of 30%. If cooling pond receives 837.2 kJ/min , what is the power developed by the cycle? Find the temp of source.

G.D :-

$$T_L = 27 + 273 = 300 \text{ K}$$

$$\eta_{th} = 30\%$$

$$Q_L = 837.2 \text{ kJ/min}$$

$$= \frac{837.2 \text{ kJ/min}}{60}$$

$$13.95 \text{ kW}$$

$$\eta_{Carnot} = \frac{T_H - T_L}{T_H}$$

$$0.3 = \frac{T_H - [300]}{T_H}$$

$$T_H =$$

Determine whether the following cases represent the reversible Irreversible or impossible heat engine

- 900 kW of heat rejected
- 560 kW " "
- 108 kW of heat rejected

In each case the engine is supplied with 1120 kJ/s of heat. Source and sink temperature are maintained at 560 K & 280 K.

O.T.D.:

$$T_1 = 560 \text{ K}$$

$$T_2 = 280$$

$$Q = 1120 \text{ kJ/s}$$

$$(i) Q_R = 900 \text{ kJ/s}$$

$$(ii) Q_R = 560 \text{ kW}$$

$$(iii) Q_R = 108 \text{ kW}$$

To find:

Concluded above cases are reversible, irreversible and impossible heat engines.

Solution:

from Carnot theorem

$$\eta_{\text{max}} = \frac{T_H - T_L}{T_H} = \frac{560 - 280}{560} = 0.5 \approx 50\%$$

(maximum efficiency is 50% value 89.96% is 21.39% engine possible practical range)

Case (i)

$$\eta_i = \frac{Q_S - Q_R}{Q_S} = \frac{1120 - 900}{1120} = 0.196 = 19.6\%$$

$\eta_i < \eta_{\text{max}}$ ∴ The engine is possible heat engine.

A heat engine of 30% efficiency drives a heat pump of COP = 5. The heat is transferred both from Engine and Heat Pump to the circulating water for heating the building in winter. Find the ratio of heat transferred to Circulating water from the heat pump to the heat transferred to the Circulating water from the heat engine.

Q. D :

$$\eta_{HE} = 30\%$$

$$COP \text{ of HP} = 5$$

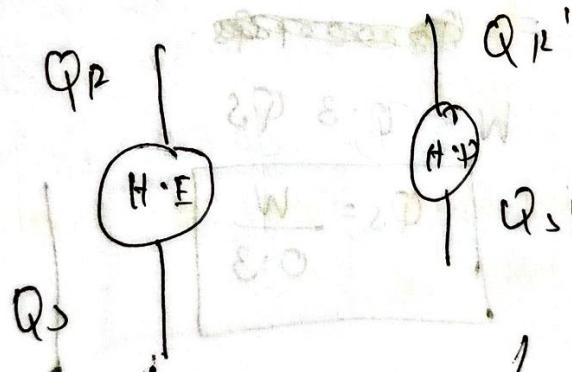
To find

$$\frac{Q_S}{Q_S'}$$

$$Q_S =$$

$$3P - 2P = Q_P - 2P = W$$

Solution:



For heat engine

$$\eta_{HE} = \frac{Q_S - Q_R}{Q_S} = 0.3$$

$$Q_S - Q_R = 0.31 Q_S$$

$$Q_S - 0.31 Q_S = 0.3 Q_S$$

(Considering adiabatic
process)
 $Q_S = 1$

$$\text{Q}_S - 0.3 \text{Q}_S = \text{Q}_R$$

For heat engine:

$$\eta_{H.E} = \frac{\text{Q}_S - \text{Q}_R}{\text{Q}_S} = 0.3$$

$$\text{Q}_S - \text{Q}_R = 0.3 \text{Q}_S$$

$$\text{Q}_R = \text{Q}_S -$$

$\text{Q}_S \text{ given } 36$
Volumetric
Efficiency

$$\text{We consider } \text{Q}_S \text{ (1)} \quad (\text{Q}_S) - 0.3 \text{Q}_S = \text{Q}_R$$

$$(1 - 0.3) \rightarrow 0.7 \text{Q}_S = \text{Q}_R$$

$$W = \text{Q}_S - \text{Q}_R = \text{Q}_S - 0.7 \text{Q}_S$$

$$W = 0.3 \text{Q}_S$$

$$\boxed{\text{Q}_S = \frac{W}{0.3}}$$

$$W = \text{Q}_P' - \text{Q}_S' = \text{Q}_S' - 0.8 \text{Q}_S'$$

$$W = 0.2 \text{Q}_S'$$

$$\text{Q}_S' = \frac{W}{0.2}$$

$$W$$

$$\therefore \frac{\text{Q}_S'}{\text{Q}_S} = \frac{0.2}{W} = \frac{0.3}{0.2} = 1.5$$

$$0.3 //$$

~~$$C.O.P = \frac{\text{Q}_S'}{\text{Q}_S' - \text{Q}_R'} = 5$$~~

~~$$\text{Q}_S' - \text{Q}_R' = \frac{\text{Q}_S'}{5}$$~~

~~$$\text{Q}_S' - \frac{\text{Q}_S'}{5} = \text{Q}_R'$$~~

~~$$\text{Q}_S' \left[1 - \frac{1}{5} \right] = \text{Q}_R'$$~~

~~$$\frac{\text{Q}_R'}{\text{Q}_S'} = 0.8$$~~

2-9

$$\eta_{H.T} = \frac{Q_S - Q_R}{Q_S} = 0.3$$

~~$$Q_S - Q_R = 0.3 \times Q_S$$~~

~~$$Q_S - 0.3 Q_S = Q_R$$~~

~~$$(1 - 0.3) Q_S = Q_R$$~~

$$0.7 Q_S = Q_R \quad \text{--- (1)}$$

$$\boxed{\frac{Q_R}{Q_S} = 0.7} \quad \text{--- (2)}$$

$$W = Q_S - Q_R \quad \text{--- (3)}$$

Sub (1) in (3)

$$W' = Q_S - 0.7 Q_S$$

$$W = 0.3 Q_S$$

$$\boxed{Q_S = \frac{W}{0.3}} \quad \text{--- (4)}$$

Heat Pump :

$$COP = \frac{Q_S'}{Q_S' - Q_R'} = 5$$

$$\boxed{\frac{Q_S'}{Q_S' - Q_R'} = \frac{5}{Q_S' - Q_R'}}$$

$$\frac{Q_S'}{5} = Q_S' - Q_R'$$

$$Q_R' = Q_S' - \frac{Q_S'}{5}$$

BOD
B
13
P
-10

$$Q_s' - \frac{Q_s'}{5} = Q_R'$$

$$Q_s' \left(1 - \frac{1}{5}\right) = Q_R'$$

$$Q_R' = Q_s' (1 - 0.2)$$

$$Q_R' = Q_s' (0.8) \quad \text{--- (5)}$$

$$\frac{Q_R'}{Q_s'} = 0.8 \quad \text{--- (6)}$$

$$W = Q_s' - Q_R' \quad \text{--- (7)}$$

Sub 5 in 7

$$W = Q_s' (0.8) - Q_s'$$

$$W = Q_s' - 0.8 Q_s'$$

$$W = 0.2 Q_s'$$

$$Q_s' = \frac{W}{0.2}$$

$$\frac{Q_s'}{Q_s} = \frac{\frac{W}{0.2}}{\frac{(W/0.3)}{(W/0.3)}} = \frac{W}{0.2} \times \frac{0.3}{W} = \frac{0.3}{0.2} = 1.5$$

$$\frac{Q_s'}{Q_s} = \frac{W}{0.2} = \frac{W \times 0.3}{0.2 \times W} = 1.5$$

$0.3 \rightarrow$ Denominator
Bun Bun unjuga so =

Concept of entropy :-

2-80

- Entropy is an index of unavailability or degradation of energy.
- It is measure molecular disorder or random function of a system process.
- It can be created but it cannot be destroyed.
- Heat always flow from hot body to cold body and thus become lesser value available. This unavailability of energy is measured by entropy.
- It is an important thermodynamics property of the working substance.

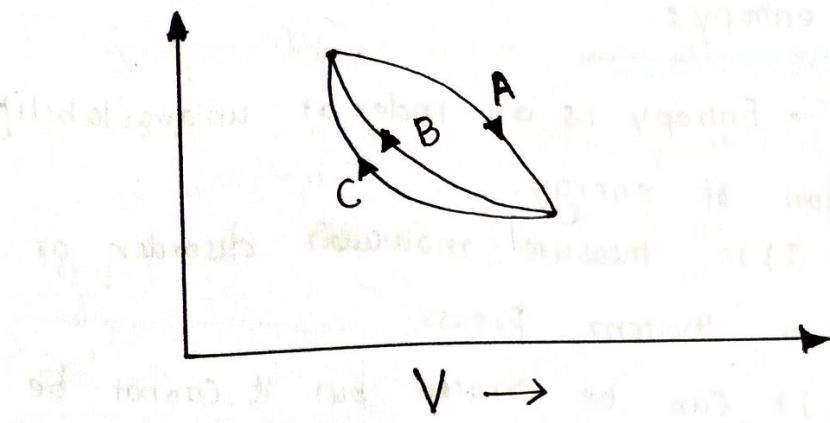
$$\text{Change in entropy } ds = \frac{\text{Change of heat transfer } (dq)}{\text{Absolute temperature } (T)}$$

Unit is kJ/K or J/K

$$\text{Change in entropy } \Delta s = S_2 - S_1 = \int_1^2 \left[\frac{dq}{T} \right]$$

Entropy : A property of the system

$$\frac{q_b}{T_2} - \frac{q_b}{T_1} = \frac{q_b}{T_2} \Delta S$$



The thermodynamic system undergoes change of state from 1 to 2 by reversible process 1-A-2 and returns to its original state 1 by another reversible process 2-B-1 and Completing cycle 1-2-1

1-2-1

For cyclic reversible processes the entropy equation is

$$\oint_{\text{rev}} \frac{dQ}{T} = 0 = \int_1^2 \frac{dQ}{T} + \int_{2B}^{1B} \frac{dQ}{T} \quad \text{--- (1)}$$

Now let us consider the cycle 1-2-1 Completed another reversible process 2-C-1

$$\text{Then } \oint_{\text{rev}} \frac{dQ}{T} = 0 = \int_1^2 \frac{dQ}{T} + \int_{2C}^{1C} \frac{dQ}{T} \quad \text{--- (2)}$$

Subtracting equation (2) from (1)

$$\int_{2B}^{1B} \frac{dQ}{T} = \int_{2C}^{1C} \frac{dQ}{T}$$

Availability:

28

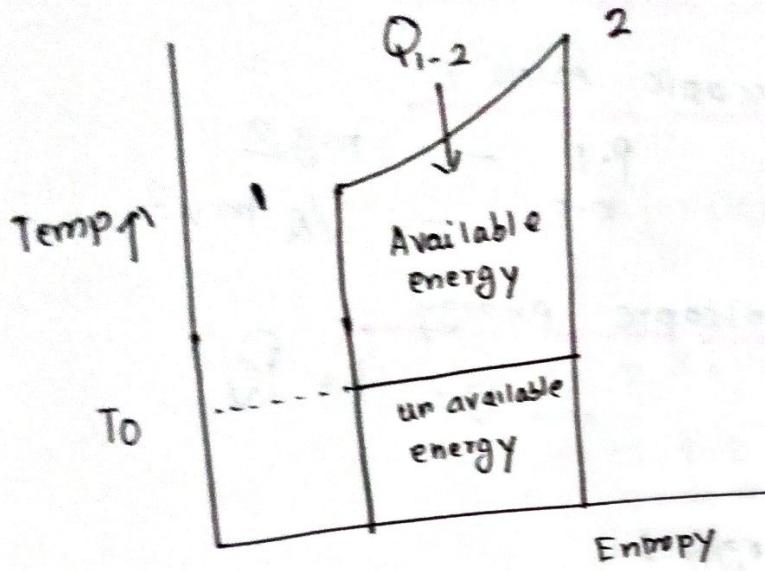
- The maximum portion of energy which could be converted into useful work and which reduces the system to a dead state.
- The portion of the available energy which is not converted to useful work is known as unavailable energy.

Available energy Referred A Cycle:

The maximum output obtainable from a certain heat input in a cyclic heat engine [reversible engine] is called the available energy

(AE).

The minimum energy loss that has to be rejected to the sink as per the second law is called unavailable energy or unavailable part of supplied energy.



2.12

2.13

$[T_2/T_1] - R$

$[P_2/P_1]$

]

2]

sounding

Classification of energy:-

Energy is defined as capacity to do work.

Energy has many form

(i) Mechanical

(2) Chemical

(3) electrical

(4) Thermal

(5) Nuclear

(6) electromagnetic

(7) Wind etc

Thermodynamic energy Classified into two type

(i) stored energy

(ii) Transit energy

Store energy has two types

200

(i) Macroscopic energy

$$P.E = mgz$$

$$K.E = \frac{1}{2}mv^2$$

(ii) Microscopic energy

$$U = h + Pv$$

Transit energy :-

The energy possessed by the system

which is capable of crossing the boundaries

FORMULA'S

Availability at Initial Ψ_1

$$mc_p(T_1 - T_0) [C_p \ln \left(\frac{T_1}{T_0} \right) - R \ln \left(\frac{P_1}{P_0} \right)]$$

Availability at final Ψ_2

$$mc_p(T_2 - T_0) [C_p \ln \left(\frac{T_2}{T_0} \right) - R \ln \left(\frac{P_2}{P_0} \right)]$$

Maximum work :

$$W = \Psi_1 - \Psi_2$$

Formulas :

2.1B

For any Process
change in entropy $\Delta s = s_2 - s_1 = m \left[c_p \ln \left[\frac{T_2}{T_1} \right] - R \ln \left[\frac{P_2}{P_1} \right] \right]$

Decrease availability $= \psi_1 - \psi_2$
 $\psi_1 - \psi_2 = m \left[h_1 - h_2 \right] - T_0 \left[s_1 - s_2 \right]$
 $= m c_p [T_1 - T_2] - T_0 [s_1 - s_2]$

Irreversibility $I = T_0 (\Delta s_{\text{system}} + \Delta s_{\text{surrounding}})$

ψ_1 Availability of hot fluid
 $\psi = m_1 \left[c_p [T_1 - T_2] - T_0 (s_1 - s_2) \right]$

$$\therefore s_1 - s_2 = c_p I n \frac{T_1}{T_2}$$

Availability of cold fluid

$$\psi_2 = m_2 \left[(h_4 - b_3) - T_0 (s_4 - s_3) \right]$$

2nd law of Efficiency η_{II} $\eta_{II} = \frac{\text{Availability of cold fluid}}{\text{Availability of hot fluid}}$

Availability at inlet $\psi_1 = h_1 - T_0 s_1$

Availability at outlet $\psi_2 = h_2 - T_0 s_1$

$$\text{The available energy} = m C_p \int_{T_0}^T \left[1 - \frac{T_0}{T} \right] dT$$

Irreversibility

$$(\Delta s)_{\text{system}} = m C_v \times \ln \left[\frac{T_2}{T_1} \right] + m R * \ln \left[\frac{V_2}{V_1} \right]$$

Irreversibility =

$$\begin{aligned} I &= T_0 \left[\Delta s_{\text{system}} + \Delta s_{\text{surrounding}} \right] \\ &= T_0 [S_2 - S_1] + \frac{Q_0}{T_0} \end{aligned}$$

Where

ψ_1 - Availability energy for Initial

ψ_2 ... final

h_1 - Enthalpy

h_2 - enthalpy

S_1 - Entropy

S_2 - entropy

T_0 = Surrounding or atmospheric temp

P_0 = " " Pressure

To Find Entropy:

$$\text{Change in Entropy } ds = m R \ln \left[\frac{V_2}{V_1} \right] + m c_v \ln \left[\frac{T_2}{T_1} \right]$$

(In terms of Volu & temp)

$$\text{Change in entropy } ds = m R \ln \left[\frac{P_1}{P_2} \right] + m c_p \ln \left[\frac{T_2}{T_1} \right]$$

(In terms of press & temp)

$$\text{Change in entropy } ds = m R \ln \left[\frac{V_2}{V_1} \right] + m c_v \ln \left[\frac{P_2}{P_1} \right]$$

Expression for the energy of an open system in terms of Availability and second law efficiency

Steady flow energy equation for any kind of Open system follows the energy balance concept

$$m \left[h_1 + \frac{c_1^2}{2} + z_1 g \right] + Q = m \left[h_2 + \frac{c_2^2}{2} + z_2 g \right] + W$$

Case (a) Turbine :-

The following assumptions are made

(i) potential energy one negligible

(ii) Inlet Velocity of the turbine is negligible

Compared to exit Velocity The S.F.E.E

When reduce

The actual work output $W_{act} = m(h_1 - h_2) + Q$

[For air $(h_1 - h_2) = C_p [T_1 - T_2]$ $Q = -ve$ when heat is transferred to the Surrounding]

Reversible work (W_{rev}) Maximum work on availability change

$$W_{max} = [h_1 - h_2] - T_0 (S_1 - S_2)$$

$$\text{Irreversibility } I = T_0 \Delta s \quad [\Delta s = S_1 - S_2]$$

Case b: Compressor / Pump:

The following assumption are made such as change in P.E & K.E are negligible therefore SFEE reduces to

$$m(h_1) + Q = m(h_2) + W$$

$$W = m(h_2 - h_1) + Q$$

Actual work input $W_{act} = m(h_2 - h_1) = Q$

[Compressor/pump are worse absorbing devices]

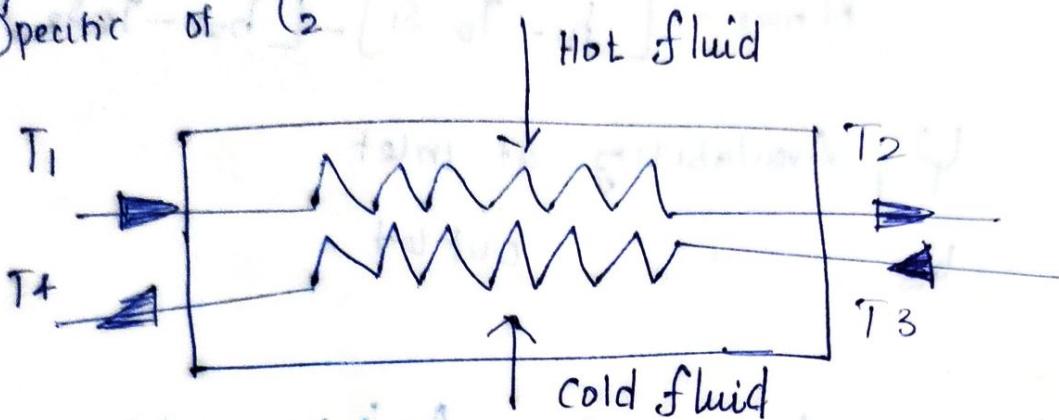
Max work input $W_{max} = m[h_2 - h_1] - T_0(S_2 - S_1)$

$$\text{Irreversibility } I = T_0 \Delta s$$

$$\text{Second law of efficiency } \eta_{II} = \frac{W_{max}}{W_{act}}$$

heat exchanger

Consider m₁ hot fluid with Specific heat of c₁
 exchanging heat with cold fluid of m₂ kg with
 specific of c₂



Heat exchanger

By heat balance

∴ heat gained by cold fluid = heat given out by hot fluid

$$m_2 c_2 [T_4 - T_3] = m_1 c_1 (T_1 - T_2)$$

Availability of cold fluid $B_c = m_2 c_2 [T_4 - T_3] - T_0 [S_4 - S_3]$

.. hot .. $B_h = m_1 c_1 [T_1 - T_2] - T_0 [S_1 - S_2]$

2nd law of efficiency $\eta_{II} = \frac{\text{Availability of cold fluid}}{\text{Availability of hot fluid.}}$

Throttling Process

Enthalpy before throttling = Enthalpy after throttling

$$h_1 = h_2$$

$$1.1 \quad h_1 - h_2 = T_0 (s_1 - s_2) + P$$

Throttling Process both work output and heat transfer are zero

$$\text{Max. Work } W_{\max} = h_1 - h_2 - T_0 [s_1 - s_2]$$

$$kW_{\max} = [h_1 - T_0 s_1] - [h_2 - T_0 s_2] = \psi_1 - \psi_2$$

ψ_1 Availability at inlet

ψ_2 " outlet

$$\text{2nd law of efficiency } \eta_{II} = \frac{\text{Availability outlet}}{\text{Availability inlet}} = \frac{\psi_2}{\psi_1}$$

At the inlet of the nozzle, the enthalpy & velocity of fluid are 3000 kJ/kg and 50 m/s respectively.

semil

There is negligible heat loss from the nozzle. At the outlet of the nozzle enthalpy is 2450 kJ/kg. If the nozzle is horizontal find the velocity of fluid at exit

Sol:C.I.D:

$$h_1 = 3000 \text{ kJ/kg}$$

$$c_1 = 50 \text{ m/s}$$

$$Q = 0; z_1 = z_2$$

$$(\text{height above datum line}) z_1 = z_2 \quad (\text{so } z_1 = z_2)$$

To findVelocity of fluid exit [c₂]

$$h_1 + \frac{c_1^2}{2} + z_1 g + Q = h_2 + \frac{c_2^2}{2} z_2 g + W$$

$$\therefore z_1 = z_2$$

$$\frac{c_1^2}{2} + h_1 + \frac{c_2^2}{2} + h_2$$

$$c_2 = \sqrt{2(h_1 - h_2) + c_1^2}$$

$$c_2 = \sqrt{2 \times (3000 - 2450) + 50^2}$$

$$c_2 = 1050 \text{ m/s}$$

$\because 1000 \text{ for molar in J/g}$

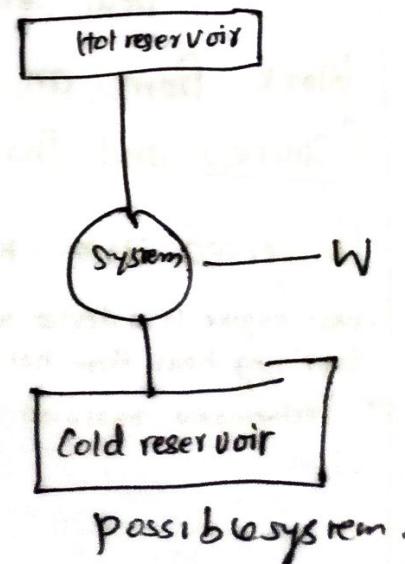
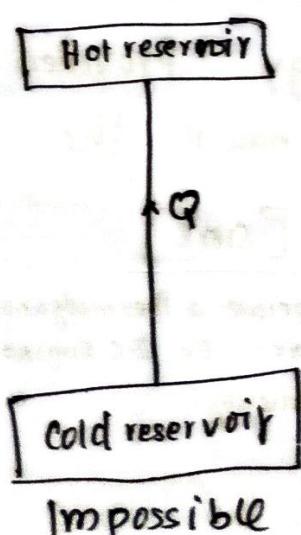
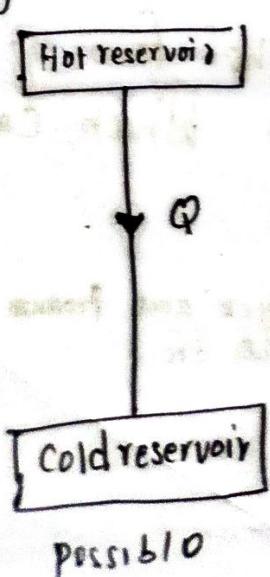
Introduction To The second Law of Thermodynamics

- A process must satisfy the ^{1st} Law of Thermodynamics to occur
- However satisfying ^{1st} law alone does not ensure that the process will actually take place.
- According to ^{1st} law of thermodynamics all form of energy are equivalent.
- One form of energy can be converted into other form and any process is possible as long as it doesn't create energy or destroy energy.

But actual practice, all form of energy can't be changed into work. Hence there are certain processes which are not possible to occur even though these processes do not violate first law of thermodynamics.

Gibbs Clausius Statement :-

- heat cannot flow from cold reservoir to hot reservoir without any external device.
- But heat can flow from hot reservoir to cold reservoir without any external aid.



Heat reservoir:-

Source :

It is the thermal energy reservoir from which the heat Q_1 is transferred to the system operating in the heat engine cycle is called Source.

Sink :

It is Thermal energy reservoir to which the heat Q_2 is rejected from the system during a cycle is called sink.
(or)

A reservoir that supplies energy in the form of heat is called a Source, and one that absorbs energy in the form of heat is called a sink. Thermal energy reservoir are often referred to as heat reservoirs since they supply or absorb energy in the form of heat.

Heat engine:-

Heat engine is used produce the maximum work from an energy provided in the form of heat (Source) and that exhausts the heat which cannot be converted into work [sink]

- p.no
2.1
- Heat engine is a device which operate a thermodynamic cycle and produce work by supplying heat from hot reservoir. Ex I.C Engine, Boiler etc..
 - Performance measured by Efficiency